

# S-ZDES: ZONAL DETACHED EDDY SIMULATION COUPLED WITH STEADY RANS IN THE WALL REGION

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# DES — DETACHED-EDDY SIMULATIONS

- Problem:

- ▶ the flow in the RANS region is highly unsteady (i.e. **URANS**)
- ▶ this means that RANS turbulence models (developed for **steady** flow) are not accurate

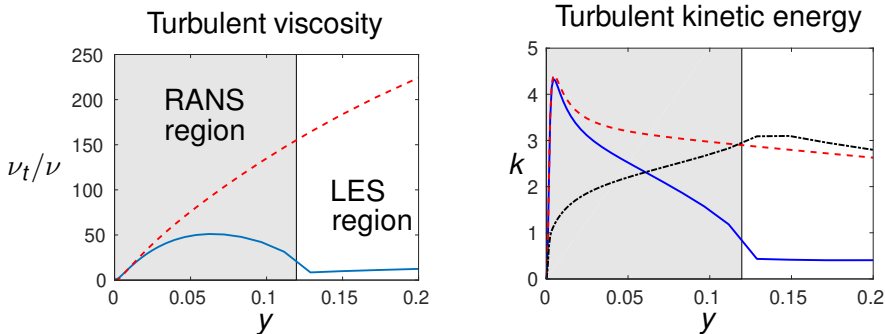


FIGURE: — : DES; - - - : 1D steady RANS; - - - : DES resolved  $k$ .

# DES — DETACHED-EDDY SIMULATIONS

- Problem:
  - ▶ the flow in the RANS region is highly unsteady (i.e. **URANS**)
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- Solution:
  - ▶ solve the **steady** equations in the RANS region

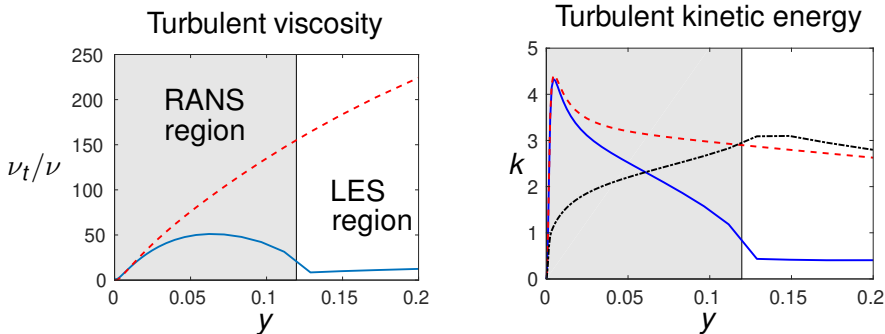


FIGURE: — : DES; - - - : 1D steady RANS; - - - : DES resolved  $k$ .

# TWO SOLVERS IN THE ENTIRE DOMAIN

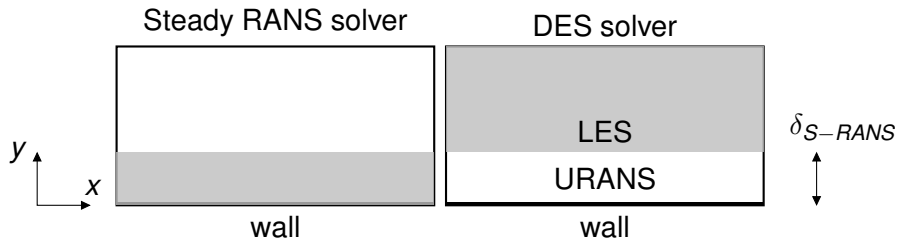


FIGURE: Grey color indicates the solver that drives the flow

# DRIFT TERMS ARE ADDED IN WHITE REGIONS



$$S_i^{RANS} = \frac{\langle v_i^{LES} \rangle_T - v_i^{RANS}}{\Delta t}$$

$$S_i^{LES} = \frac{v_i^{RANS} - \langle \bar{v}_i^{LES} \rangle_T}{\Delta t},$$

FIGURE: Subscript  $T$  indicates integration over time  $T$

$$\langle \phi(t) \rangle_T = \frac{1}{T} \int_{-\infty}^t \phi(\tau) \exp(-(t-\tau)/T) d\tau \Rightarrow$$
$$\langle \phi \rangle_T^t \equiv \langle \phi \rangle_T = a \langle \phi \rangle_T^{t-\Delta t} + (1-a) \phi^t$$
$$a = \exp(-\Delta t/T).$$

## PREVIOUS WORK

- The present method is similar to those in [1, 2, 3]. The main differences are that
  - ▶ In [1, 3] they use one **additional** drift terms in the LES momentum equations to control resolved Reynolds stresses
  - ▶ They include drift terms also in the  $k$  and  $\varepsilon$  equations [1] or the  $k$  equation [3].
  - ▶ In [1, 3] they include **five** tuning constants in all drift terms. I have **one** ( $T$ ).

# TURBULENCE MODELS



- EARSM (Explicit Algebraic Stress Model) [4] coupled to Wilcox  $k - \omega$  model [5]
- DES  $k - \omega$  model
- Lengthscale in dissipation term of the  $k$  eq. is taken from the IDDES model [6, 7]

FIGURE: RANS and DES turbulence models

# NUMERICAL METHOD: CALC-LES & CALC-BFC

- CALC-LES [8]: DES solver
  - ▶ Incompressible finite volume method
  - ▶ Pressure-velocity coupling treated with fractional step
  - ▶ Central differencing scheme for momentum eqns
  - ▶ Hybrid 1<sup>st</sup> order upwind/2<sup>nd</sup> order central scheme  $k$  &  $\omega$  eqns.
  - ▶ 2<sup>nd</sup>-order Crank-Nicholson for time discretization
- CALC-BFC [9]: RANS solver, called every 10<sup>th</sup> timestep
  - ▶ Incompressible finite volume method
  - ▶ SIMPLEC
  - ▶ MUSCL: 2nd order bounded upwind scheme for momentum eqns
  - ▶ Hybrid 1<sup>st</sup> order upwind/2<sup>nd</sup> order central scheme  $k$  &  $\omega$  eqns.



# FIRST TEST CASE: CHANNEL FLOW

- Reynolds number is  $Re_\tau = 5200$ .
- A  $32 \times 96 \times 32$  mesh is used
- $x_{max} = 3.2$ ,  $z_{max} = 1.6$ , 15% stretching in  $y$  direction

# CHANNEL FLOW: VELOCITY

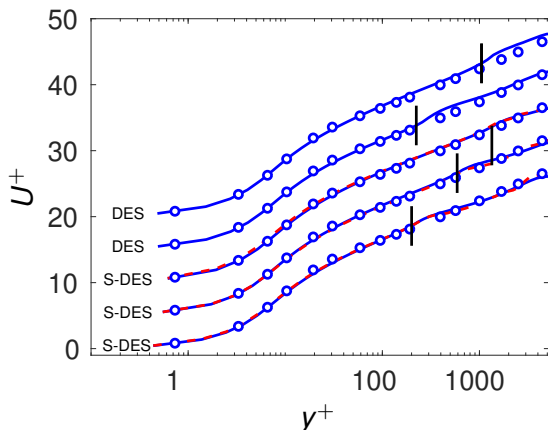


FIGURE:  $T = 10\delta/U_b$  — : DES; - - : RANS; ○ : DNS. Vertical black lines show locations of  $\delta_{S-RANS}$ .

# CHANNEL FLOW: TURBULENT VISCOSITY

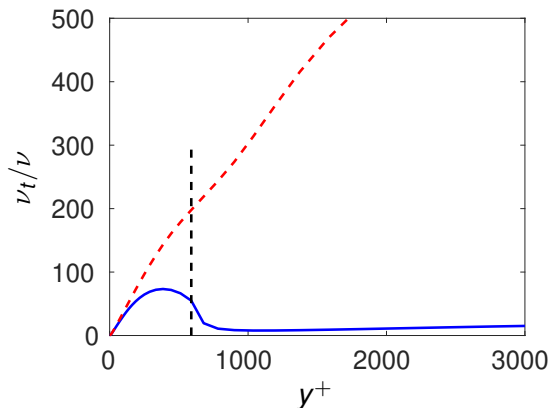


FIGURE: — : DES solver; - - : RANS solver. Vertical black lines show locations of  $\delta_{S-RANS}$ .

## SECOND TEST CASE: HUMP FLOW

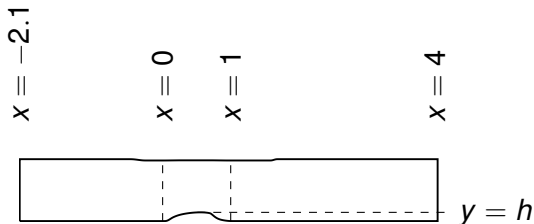
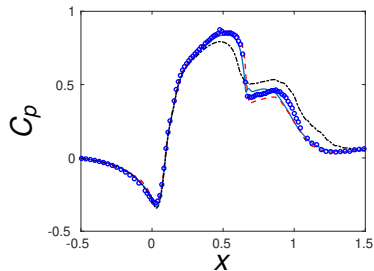


FIGURE: The domain of the hump.  $z_{max} = 0.2$ .

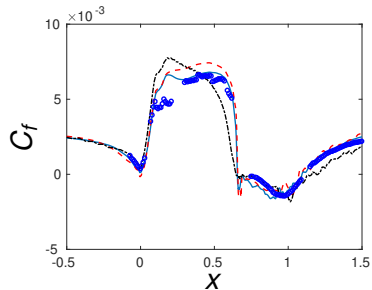
- The Reynolds number of the hump flow is  $Re_c = 936\,000$ .
- The mesh has  $386 \times 120 \times 32$  cells ( $x, y, z$ )
- Grid from NASA workshop.<sup>1</sup>
- Inlet is located at  $x = -2.1$  and the outlet at  $x = 4.0$ ,

<sup>1</sup>[https://turbmodels.larc.nasa.gov/nasahump\\_val.html](https://turbmodels.larc.nasa.gov/nasahump_val.html)

# HUMP FLOW: $C_p$ & $C_f$



(A) Pressure coefficient.



(B) Skinfriction.

FIGURE:  $T = 20h/U_{in}$ . — : S-DES,  $j_0 = 33$ ; - - : S-DES,  $j_0 = 53$ ; - - - : DES

# HUMP FLOW: VELOCITIES

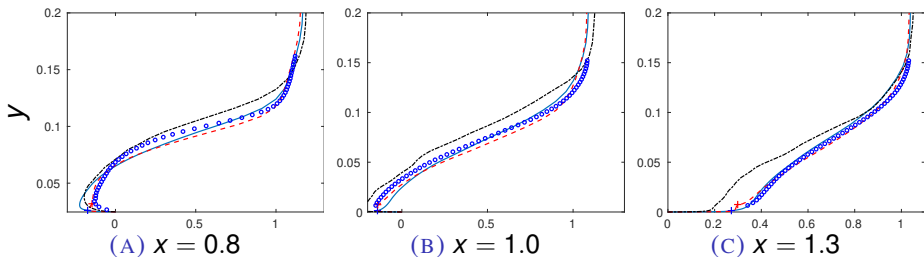


FIGURE: — : S-ZDES,  $j_0 = 33$ ; - - : S-ZDES,  $j_0 = 53$ ; - · - : DES; ○ : exp

# CONCLUSIONS

- A new **steady** RANS coupled to **DES (S-ZDES)** is proposed.
- Very good results
- Drawback: it is dependent on the **lower limit** of integration time,  $T$  for the hump flow
  - ▶  $T = 10h/U_{in}$  too small ( $h$  is hump height)
  - ▶  $T = 20$  and  $50$  give identical results
  - ▶ For  $T = 100$  we must more than double developing+sampling time to  $345 + 345$  ( $7.3 + 7.3$  throughflow times)

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