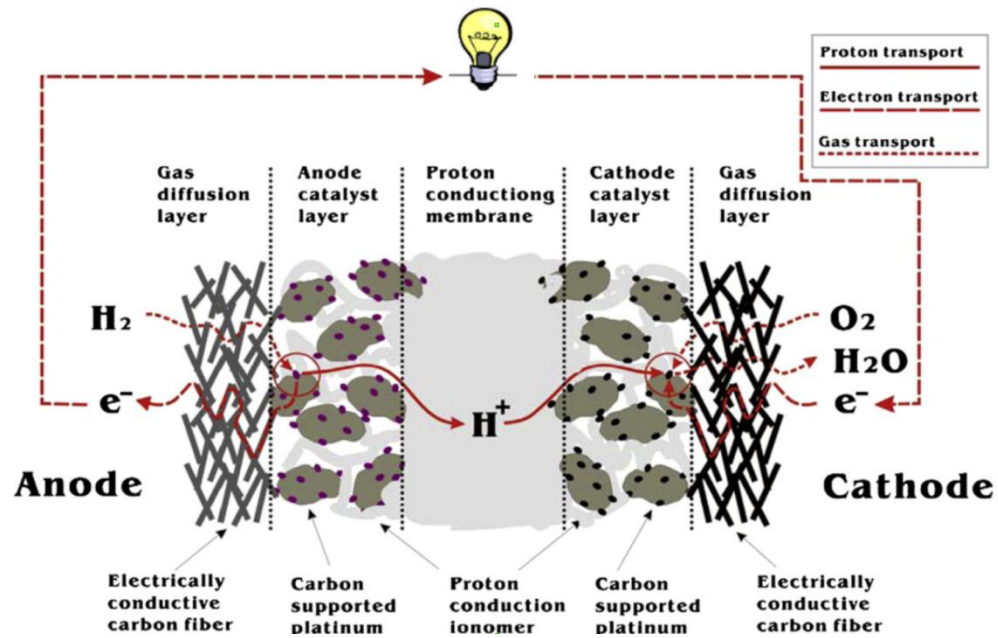
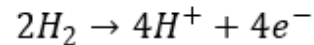


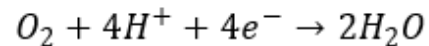
# How fuel cells work



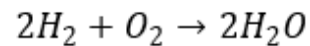
Anode side reaction:



Cathode side reaction:



Net reaction:

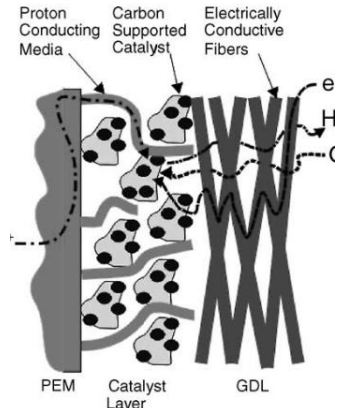


- A fuel cell is a device that converts chemical potential energy into electrical energy

- A PEM (Proton Exchange Membrane) cell uses hydrogen gas (H<sub>2</sub>) and oxygen gas (O<sub>2</sub>) as fuel

- The products of the reaction in the cell are water, electricity, and heat

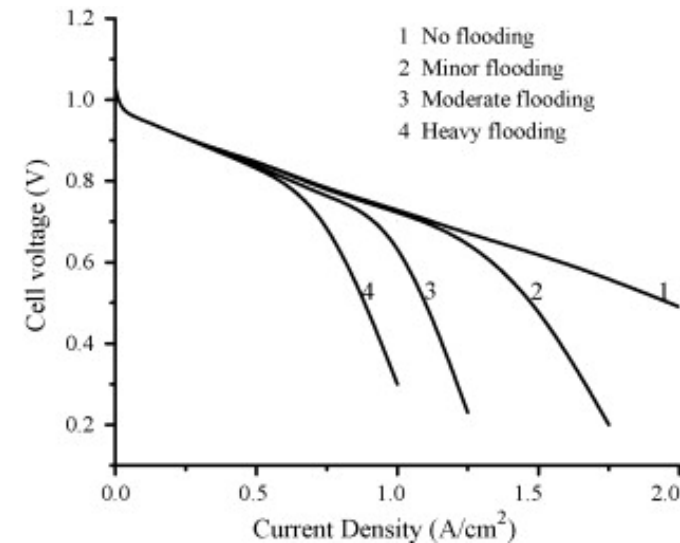
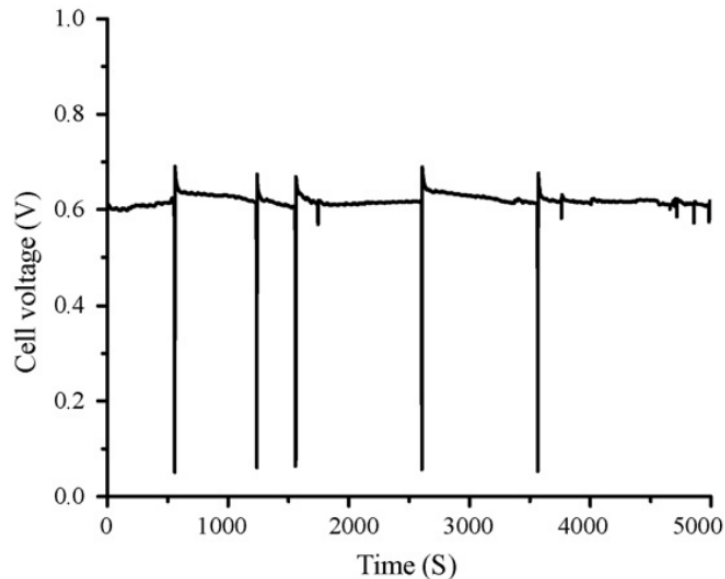
# Water flooding in fuel cells



-Hydration is necessary for fuel cell operation

- Excess water fills the pores and blocks the access of reactants

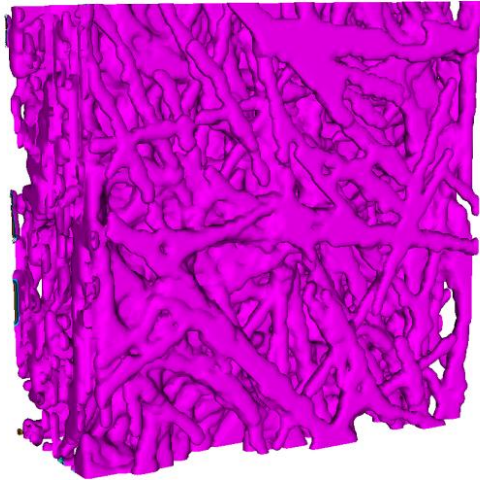
-Water management influences cell efficiency



A typical water flooding pattern in a PEM fuel cell

Polarization curves of a PEM fuel cell: the effect of water flooding

# Modeling of water flow dynamics in GDL



## Carbon cloth and carbon paper for Gas Diffusion Layer (GDL)

Thickness: 200-400 micron

Fiber diameter: ~10 micron

Pore size: ~80 micron

## Goal:

Modeling of two-phase flows in a real GDL structure

Pore-scale-based models for water transport and perspectives on design

Develop fuel cells with optimized geometry and water management parameters

# Lattice Boltzmann Method (LBM)

- Ideal to handle complicated boundary porous media
- Ideal to handle complex flows e.g. multiphase
- Easy for parallel computing

## Boltzmann's equation:

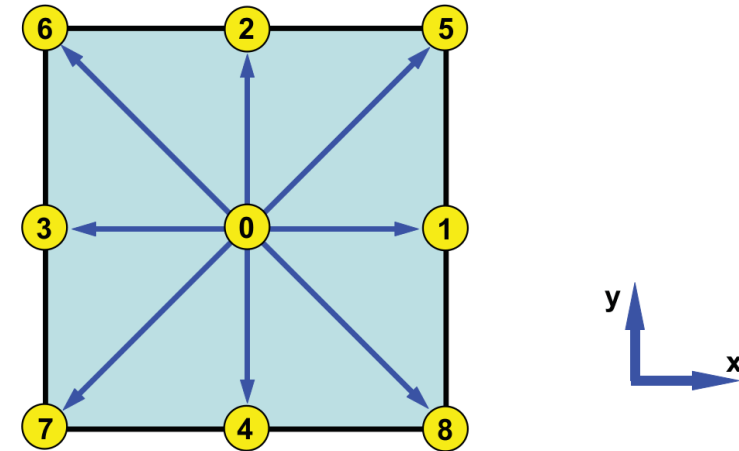
$$\frac{\partial F_i}{\partial t} + \mathbf{c}_i \cdot \hat{\nabla} F_i = -\frac{1}{\hat{\tau} \cdot \varepsilon} (F_i - F_i^{(eq)})$$

$$F_i(\mathbf{x} + \mathbf{c}_i \cdot \Delta t, t + \Delta t) - F_i(\mathbf{x}, t) = -\frac{1}{\tau} (F_i - F_i^{(eq)})$$

## Macroscopic quantities:

$$\rho(\mathbf{x}, t) = \sum_i F_i(\mathbf{x}, t)$$

$$\mathbf{j}(\mathbf{x}, t) = \rho(\mathbf{x}, t) \cdot \mathbf{u}(\mathbf{x}, t) = \sum_i \mathbf{c}_i \cdot F_i(\mathbf{x}, t)$$

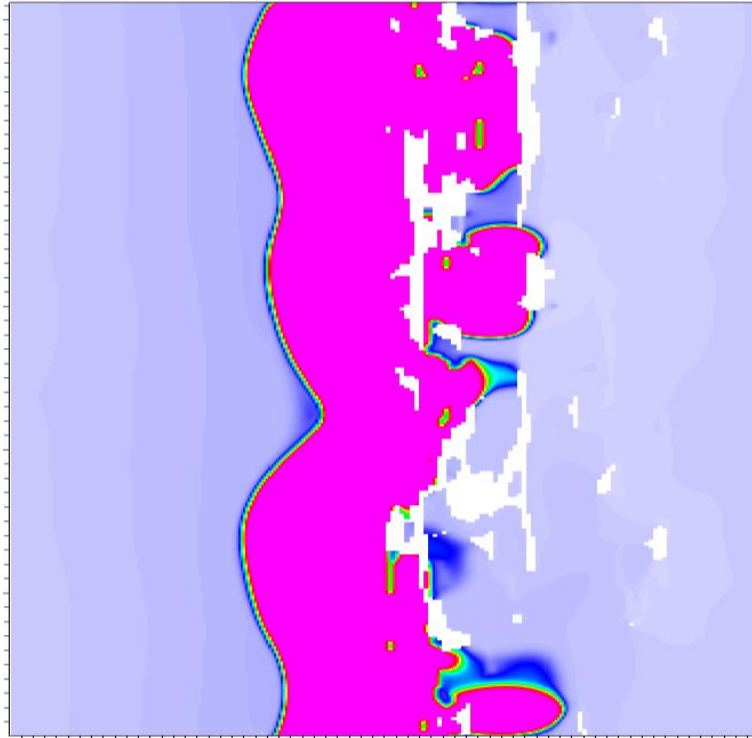


D2Q9 lattice scheme

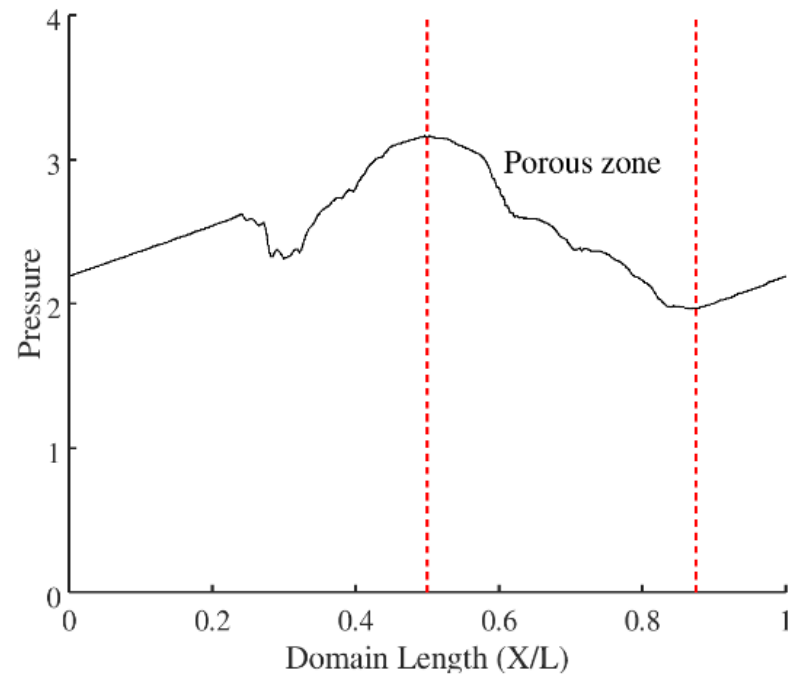
\* LBM assumes that particles are constrained to move in a lattice

# Results: Pressure variation along GDL

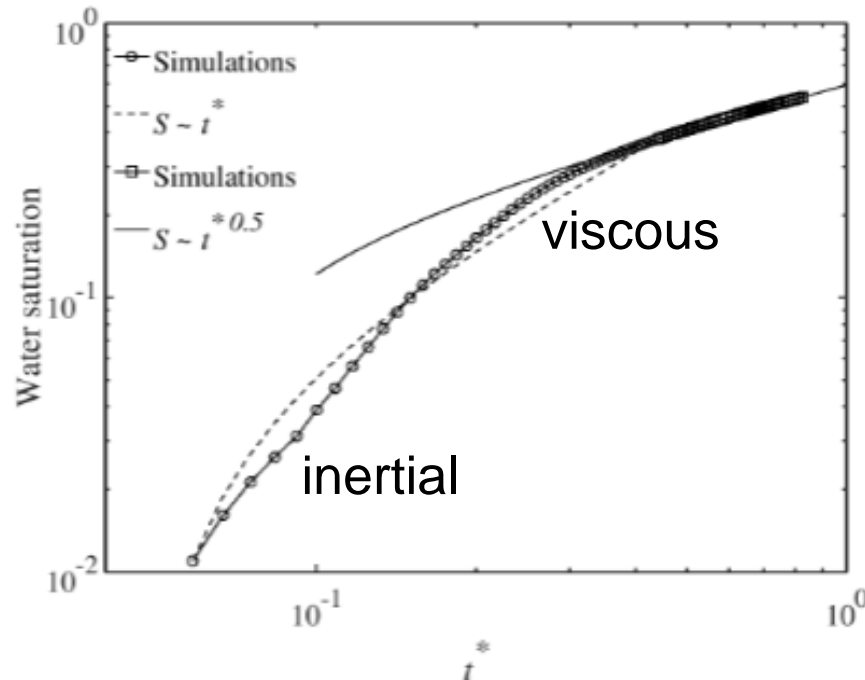
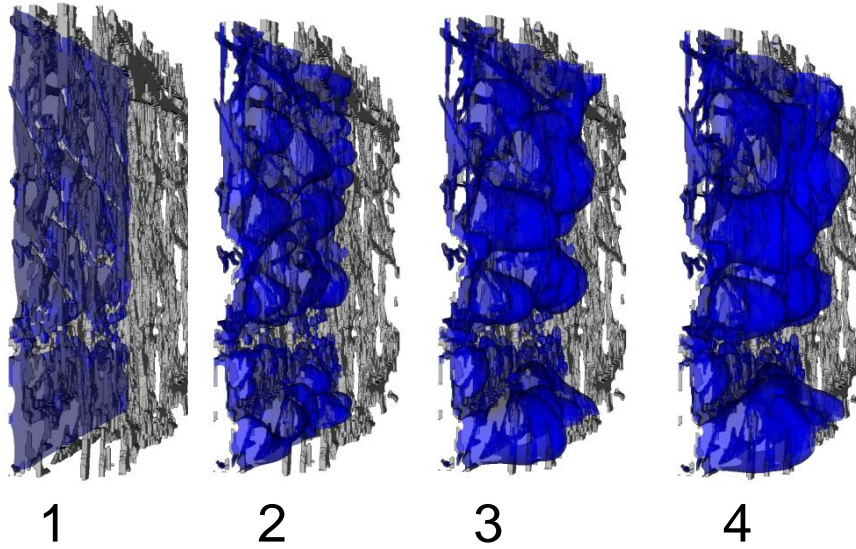
- Pressure drop is applied on the flow
- Pressure increases behind the GDL until it starts to penetrate
- Pressure decreases in porous zone



Flow distribution

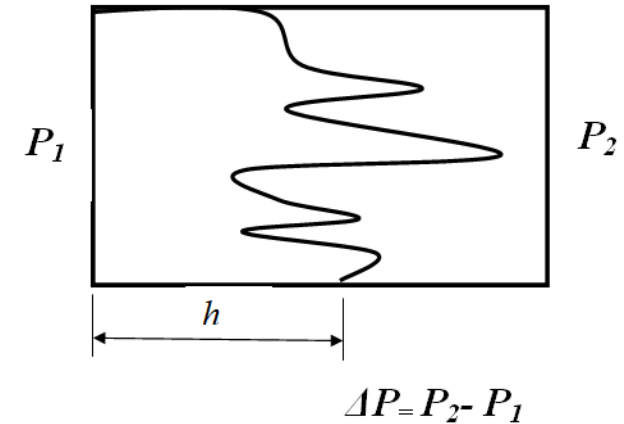


# Results: Liquid propagation in GDL



Conventional approach:

Flow in porous media is described by **Darcy's law**:



$$\bar{V} = \frac{K}{\mu_w} \frac{\Delta P}{h}$$

$$\frac{h}{t} = \frac{K}{\mu_w} \frac{\Delta P}{h}$$

$$h = \sqrt{\left(\frac{K}{\mu_w} \Delta P\right) t}$$

$$S \sim \sqrt{t}$$

# Summary

- Fuel cells description
- Water management in fuel cells
- Results of LBM simulations
- Models developed for both inertial & viscous regimes
- Darcy's Law cannot capture liquid kinetics in inertial regime